

APPENDIX 1 - Monitoring Schedule, Calibration Checklist & Monitoring Team

STACK EMISSIONS MONITORING TEAM

Team Leader

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APPENDIX 2 - Summaries, Calculations, Raw Data and Charts

TOTAL PARTICULATE MATTER SUMMARY

Parameter	Sampling Time	Concentration mg/m ³	Uncertainty mg/m ³	Limit mg/m ³	Emission Rate g/hr
Run 1	09:57 - 10:29 07 November 2013	15.5	1.74	50	794
Blank	-	0.84	-	-	-

Reference conditions are 273K, 101.3kPa without correction for water vapour

Acetone Blank Value mg/l	Acceptance Value mg/l
2.0	10

FILTER INFORMATION

Samples

Test	Filter & Probe Rinse Number	Filter Start Weight	Filter End Weight	Mass Gained on Filter	Probe Rinse Start Weight	Probe Rinse End Weight	Mass Gained on Probe	Combined Total Mass Gained
Run 1	115513.00	0.14630	0.14880	0.00250	71.02480	71.03150	0.00670	0.00920

If total mass gained is less than the LOD then the LOD is reported

Blanks

Test	Filter & Probe Number	Filter Start Weight	Filter End Weight	Mass Gained Filter	Probe Start Weight	Probe End Weight	Mass Gained Probe	Combined Total Mass Gained
Run 1	115512	0.14740	0.14760	0.00020	72.45820	72.45830	0.00010	0.00050

If total mass gained is less than the LOD then the LOD is reported

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ISOKINETIC SAMPLING EQUATIONS - RUN 1			TPM
Absolute pressure of stack gas, P_s			
Barometric pressure, P _b	mm Hg	751.51	
Stack static pressure, P _{static}	mm H ₂ O	5.10	
$P_s = P_b + (P_{static})$	mm Hg	751.88	
		13.6	
Vol. of water vapour collected, V_{wetd}			
Moisture trap weight increase, V _{lc}	g	46.7	
$V_{wetd} = (0.001246)(V_{lc})$	m ³	0.0581882	
Volume of gas metered dry, V_{mstd}			
Volume of gas sample through gas meter, V _m		0.527	
Gas meter correction factor, Y _d		1.0766	
Mean dry gas meter temperature, T _m		14.625	
Mean pressure drop across orifice, ΔH	mmH ₂ O	36.092	
$V_{mstd} = \frac{(0.3592)(V_m)(P_b + (\Delta H/13.6))(Y_d)}{T_m + 273}$		0.534	
Volume of gas metered wet, V_{matw}			
$V_{matw} = V_{mstd} + V_{wetd}$	m ³	0.5924	
Vol. of gas metered at O₂ Ref. Cond., V_{mstd@X%O2}			
Is the process burning hazardous waste? (if yes, no favourable oxygen correction)	No		
% oxygen measured in gas stream, act%O ₂	21.0		
% oxygen reference condition	21		
O ₂ Reference O ₂ Ref = 21.0 - act%O ₂	No O2 Ref		
Factor $\frac{21.0 - ref\%O_2}{21.0 - act\%O_2}$			
$V_{mstd@X\%oxygen} = (V_{mstd}) (O_2 Ref)$	m ³	No O2 Ref	
Moisture content, B_{wo}			
$B_{wo} = \frac{V_{wetd}}{V_{mstd} + V_{wetd}}$	%	0.0982	
		9.82	
Moisture by FTIR			
	%	-	
Velocity of stack gas, V_s			
Pitot tube velocity constant, K _p		34.97	
Velocity pressure coefficient, C _p		0.84	
Mean of velocity heads, ΔP _{avg}	mm H ₂ O	20.13	
Mean square root of velocity heads, √ΔP		4.49	
Mean stack gas temperature, T _s	°C	83	
$V_s = \frac{(K_p)(C_p)(\sqrt{\Delta P})(\sqrt{T_s + 273})}{(M_s)(P_s)}$	m/s	16.55	
Molecular weight of dry gas, M_d			
CO ₂	%	15.50	
O ₂	%	21.00	
Total	%	36.50	
N ₂ (100 - Total)	%	63.50	
$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2)$		31.32	
Molecular weight of wet gas, M_w			
$M_w = M_d(1 - B_{wo}) + 18(B_{wo})$	g/gmol	30.01	
Actual flow of stack gas, Q_a			
Area of stack, A _s	m ²	1.13	
$Q_a = (60)(A_s)(V_s)$	m ³ /min	1122.9	
Total flow of stack gas, Q			
Conversion factor (K/mm.Hg)		0.3592	
$Q_{std} = \frac{(Q_a)P_s(0.3592)(1 - B_{wo})}{(T_s) + 273}$	Dry	768.8	
$Q_{std@O_2} = \frac{(Q_a)P_s(0.3592)(1 - B_{wo})(O_2 REF)}{(T_s) + 273}$	@O ₂ ref	No O2 Ref	
$Q_{std@} = \frac{(Q_a)P_s(0.3592)}{(T_s) + 273}$	Wet	852.50	
Percent isokinetic, %I			
Nozzle diameter, D _n	mm	5.35	
Nozzle area, A _n	mm ²	22.48	
Total sampling time, θ	min	32	
$\%I = \frac{(4.6398E6)(T_s + 273)(V_{mstd})}{(P_s)(V_s)(A_n)(\theta)(1 - B_{wo})}$	%	109.2	
Acceptable isokinetic range 95% to 115%		Yes	
Particulate Concentration, C			
Mass collected on filter, M _f	g	0.00250	
Mass collected in probe, M _p	g	0.00670	
Total mass collected, M _n	g	0.00920	
$C_{wet} = \frac{M_n}{V_{matw}}$	mg/m ³	15.530	
$C_{dry} = \frac{M_n}{V_{mstd}}$	mg/m ³	17.222	
$C_{dry@X\%O_2} = \frac{M_n}{V_{mstd@X\%oxygen}}$	mg/m ³	No O2 Ref	
Particulate Emission Rates, E			
$E = [(C_{wet})(Q_{std})(60)] / 1000$		794.38	

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TOTAL PARTICULATE MATTER QUALITY ASSURANCE CHECKLIST

Leak Rate

Run	Mean Sampling Rate litre/min	Pre-sampling Leak Rate litre/min	Post-sampling Leak Rate litre/min	Maximum Vacuum mm hg	Acceptable Leak Rate litre/min	Leak Tests Acceptable?
Run 1	17.72	0.11	0.12	-279.4	0.35	Yes

Isokineticity

Run	Isokinetic Variation %	Acceptable Isokineticity
Run 1	109.25	Yes

Acceptable isokinetic range 95% to 115%

Balance Uncertainty

Run	Result mg/m ³	5% ELV mg/m ³	LOD < 5% ELV
Run 1	0.84	2.5	Yes

The above is based on both the Filter and rinse uncertainty

Blank Value

Run	Overall Blank Value mg/m ³	Daily Emission Limit Value mg/m ³	Acceptable Blank Value mg/m ³	Overall Blank Acceptable
Blank 1	0.84	50	5.0	Yes

Filters

Run	Filter Material	Filter Size mm	Max Filtration Temperature °C	Pre-use Filter Conditioning Temperature °C	Post-use Filter Conditioning Temperature °C
Run 1	QF	47	84	180	160

GF = Glass Fibre
QF = Quartz Fibre

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MOISTURE CALCULATIONS

Moisture Determination - Isokinetic

Test Number	Sampling Time and Date	Start Weight	End Weight	Total gain	Concentration	LOD	Uncertainty
		kg	kg	kg	%	%	%
Run 1	09:57 - 10:29 07 November 2013	4.0207	4.0674	0.0467	9.8226	0.021	2.8

Moisture Quality Assurance

Test Number	Sampling Duration	Total Volume Sampled	Sampling Rate	Start Leak Rate	End Leak Rate	Acceptable Leak Rate	Leak Tests Acceptable?
	mins	l	l/min	l/min	l/min	l/min	
Run 1	32	592	17.7249	0.1100	0.1200	0.3545	Yes

PRELIMINARY STACK SURVEY

Stack Characteristics

Stack Diameter / Depth, D	1.20	m
Stack Width, W	-	m
Stack Area, A	1.13	m ²
Average stack gas temperature	82	°C
Stack static pressure	0.05	kPa
Barometric Pressure	99.8	kPa
Pitot tube calibration coefficient, K _{pr}	0.82	-

Stack Gas Composition & Molecular Weights

Component	Molar Mass	Density	Conc Dry	Dry Volume Fraction	Dry Conc	Conc Wet	Wet Volume Fraction	Wet Conc
	M	kg/m ³ ρ	% Vol	r	kg/m ³ p _i	% Vol	r	kg/m ³ p _i
CO ₂	44	1.963059	15.500000	0.155000	0.304274	13.977500	0.139775	0.274387
O ₂	32	1.427679	21.000000	0.210000	0.299813	18.937258	0.189373	0.270363
N ₂	28	1.249219	63.500000	0.635000	0.793254	57.262660	0.572627	0.715336
H ₂ O	18	0.803070	-	-	-	9.822582	0.098226	0.076882

Where: $\rho = M / 22.41$ $p_i = r \times \rho$

Calculation of Stack Gas Densities

Determinand	Result	Units
Dry Density (STP), P _{STD}	1.3973	kg/m ³
Wet Density (STP), P _{STW}	1.3390	kg/m ³
Dry Density (Actual), P _{Actual}	1.0604	kg/m ³
Average Wet Density (Actual), P _{ActualW}	1.016	kg/m ³

Where:

P_{STD} = sum of component concentrations, kg/m³ (not including water vapour)

P_{STW} = (P_{STD} + p_i of H₂O) / (1 + (p_i of H₂O / 0.8036))

P_{Actual} = P_{STD} x (Ts / Ps) x (Pa / Ta)

P_{ActualW} = P_{STW} x (Ts / Ps) x (Pa / Ta)

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PRELIMINARY STACK SURVEY

TRAVERSE 1

Date of Survey	07 November 2013
Time of Survey	09:25
Velocity Measurement Device:	S-Type

Sampling Line A							
Traverse Point	Distance into duct (m)	ΔP_{pt} mmH ₂ O	ΔP_{pt} Pa	Temp °C	Velocity m/s	O ₂ % Vol	Angle of Swirl °
1	0.06	23.0	225	82	16.92	-	0
2	0.18	22.0	216	84	16.60	-	0
3	0.30	22.5	221	81	16.71	-	0
4	0.42	23.5	230	80	17.06	-	0
5	0.54	22.0	216	83	16.57	-	0
6	0.66	24.0	235	81	17.26	-	0
7	0.78	24.5	240	82	17.47	-	0
8	0.90	22.5	221	80	16.69	-	0
9	1.02	22.0	216	83	16.57	-	0
10	1.14	23.0	225	80	16.87	-	0
Mean	-	22.9	224	82	16.87	-	-

Sampling Line B							
Traverse Point	Distance into duct (m)	ΔP_{pt} mmH ₂ O	ΔP_{pt} Pa	Temp °C	Velocity m/s	O ₂ % Vol	Angle of Swirl °
1	-	-	-	-	-	-	-
2	-	-	-	-	-	-	-
3	-	-	-	-	-	-	-
4	-	-	-	-	-	-	-
5	-	-	-	-	-	-	-
6	-	-	-	-	-	-	-
7	-	-	-	-	-	-	-
8	-	-	-	-	-	-	-
9	-	-	-	-	-	-	-
10	-	-	-	-	-	-	-
Mean	-	-	-	-	-	-	-

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PRELIMINARY STACK SURVEY (CONTINUED)

Sampling Plane Validation Criteria

EA Technical Guidance Note (Monitoring) M1	Result	Units	Requirement	Compliant
Lowest Differential Pressure	215.6	Pa	>= 5 Pa	Yes
Lowest Gas Velocity	16.57	m/s	-	-
Highest Gas Velocity	17.47	m/s	-	-
Ratio of Gas Velocities	1.05	-	< 3 : 1	Yes
Maximum angle of flow with regard to duct axis	0	°	< 15°	Yes
No local negative flow	Yes	-	-	Yes

Other Sampling Method Criteria	Result	Units	Requirement	Compliant
Mean Velocity	16.87	m/s	-	-
Standard Deviation of Velocity from Mean	1.82	%	< 10%	Yes
Mean Oxygen	-	%	-	-
Standard Deviation of Oxygen from Mean	-	%	< 15%	-
Homogeneous flow stream / gas velocity	-	-	-	Yes

Calculation of Stack Gas Velocity, V

Velocity at Traverse Point, $V = K_{pt} \times (1-\epsilon) \times \sqrt{2 \times \Delta P_{pt} / \rho_{ActualW}}$

Where:

K_{pt} = Pitot tube calibration coefficient

(1-ε) = Compressibility correction factor, assumed at a constant 0.998

Average Stack Gas Velocity, V_a 16.87 m/s

Calculation of Stack Gas Volumetric Flowrate, Q

Duct gas flow conditions	Actual	Reference	Units
Temperature	82	0	°C
Total Pressure	99.85	101.3	kPa
Oxygen	21.0	21	%
Moisture	9.82	9.82	%

Gas Volumetric Flowrate	Result	Units
Average Stack Gas Velocity (V_a)	16.87	m/s
Stack Area (A)	1.13	m ²
Gas Volumetric Flowrate (Actual), Q_{Actual}	68707	m ³ /hr
Gas Volumetric Flowrate (STP, Wet), Q_{STP}	52139	m ³ /hr
Gas Volumetric Flowrate (STP, Dry), $Q_{STP,Dry}$	47018	m ³ /hr
Gas Volumetric Flowrate (REF), Q_{Ref}	52139	m ³ /hr

Where:

$Q_{Actual} = V_a \times A \times 3600$

$Q_{STP} = Q (Actual) \times (T_s / T_a) \times (P_a / P_s) \times 3600$

$Q_{STP,Dry} = Q (STP) / (100 - (100 / Ma)) \times 3600$

$Q_{Ref} = Q (STP) \times ((100 - Ma) / (100 - Ms)) \times ((20.9 - O_{2a}) / (20.9 - O_{2s}))$

Nomenclature:

T_s = Absolute Temperature, Standard Conditions, 273 K

P_s = Absolute Pressure, Standard Conditions, 101.3 kPa

T_a = Absolute Temperature, Actual Conditions, K

P_a = Absolute Pressure, Actual Conditions, kPa

Ma = Water vapour, Actual Conditions, % Vol

Ms = Water vapour, Reference Conditions, % Vol

O_{2a} = Oxygen, Actual Conditions, % Vol

O_{2s} = Oxygen, Reference Conditions, % Vol

